

**Errata to  
Fundamentals of Refrigeration Self-Directed Learning Course,  
I-P Edition (2010)**

**May 23, 2019**

*Shaded items have been added since the previously published errata sheet dated September 21, 2018.*

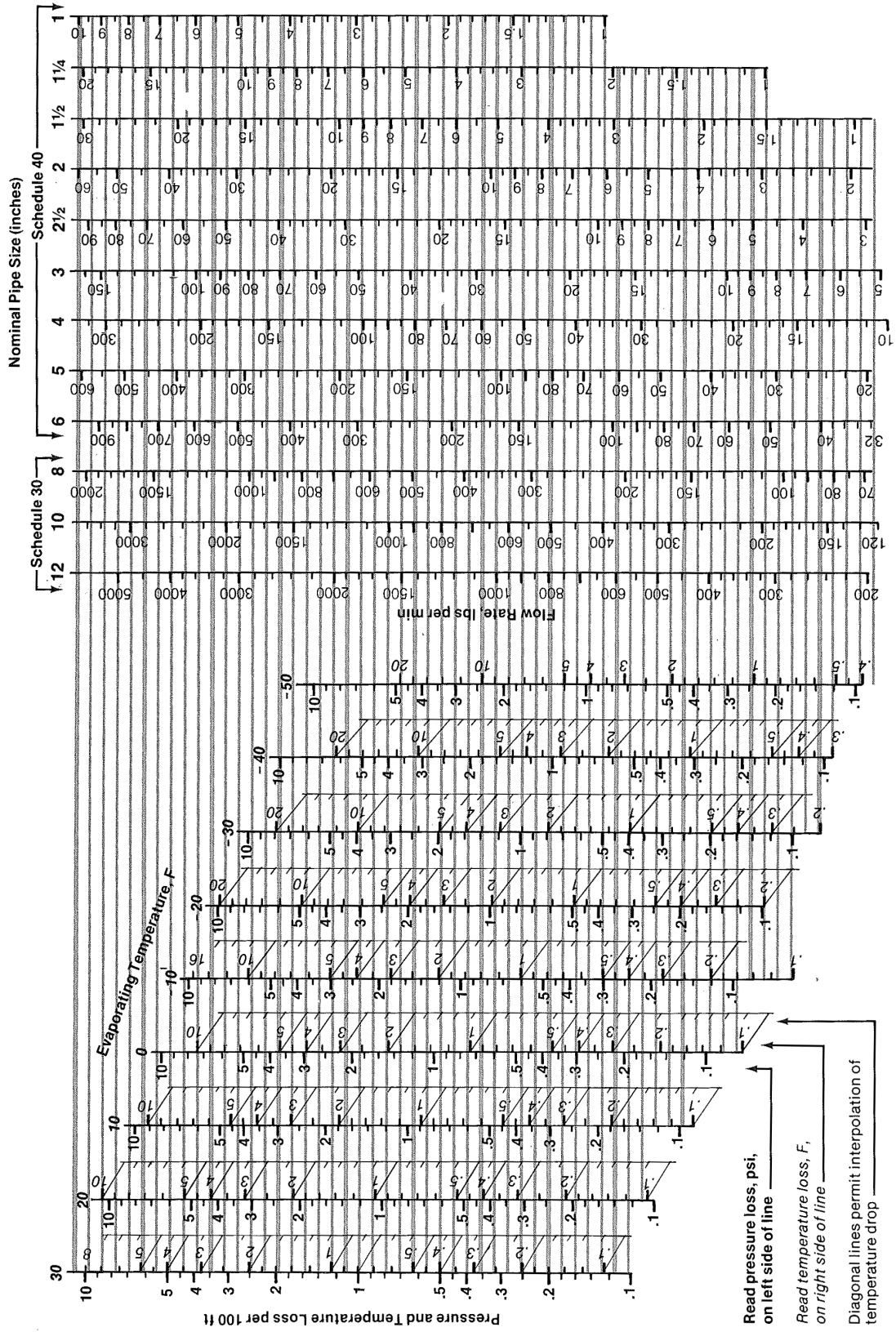
Page #	Location	
1	9 lines from bottom	Add the word “be” in the sentence that ends on this line, as in “means by which heat can be moved away.”
9	18 lines from top	“The necessary low pressure is produced by the low pressure of the refrigerant maintained by the compressor” should read “The necessary low pressure is produced by <b>the expansion device.</b> ”
21	5 lines from top	Added “(Specific heat of air at constant pressure is 0.2359 Btu/lb).”
25	3 lines from bottom	$h_g = 111.530 \text{ Btu/lb}$
25	2 lines from bottom	$h_f = 34.859 \text{ Btu/lb}$
25	bottom line	$x = (88.414 - 34.859)/(111.530 - 34.859) = 0.700$
26	4 lines from top	$\rho_f = 73.23 \text{ lb/ft}^3$
26	5 lines from top	$v_f = 1/73.23 = 0.01366 \text{ ft}^3/\text{lb}$
26	6 lines from top	$v_g = 0.3207 \text{ ft}^3/\text{lb}$
26	7 lines from top	$v = 0.01366 + (0.700)(0.3207 - 0.01366)$
26	8 lines from top	$= 0.229 \text{ ft}^3/\text{lb}$
26	6 lines from bottom	$h = 59.103 \text{ Btu/lb}$ $v = 1/40.66 = 0.02459 \text{ ft}^3/\text{lb}$
35		Update Figure 2-10 to the following:
		<b>Figure 2-10 Ideal compressor.</b>
35	Equation 2-17	$-\dot{W}_{out} = \dot{m}_2 h_2 - \dot{m}_1 h_1$
36	4 lines from top	$h_1 = 107.471 \text{ Btu/lb} \quad s_1 = s_2 = 0.22278 \text{ Btu/lb}\cdot^\circ\text{R}$
36	6 lines from top	$0.22278 \text{ Btu/lb}\cdot^\circ\text{R}$
36	12 lines from top	$T = T_{sat} = 105.17^\circ\text{F}$
36	13 lines from top	$s$ should be 0.22278
36	15 lines from top	$h_2 = 116.71 + \frac{(0.22278 - 0.21844)}{(0.22530 - 0.21844)}(120.64 - 116.71)$
36	16 lines from top	$= 119.20 \text{ Btu/lb}$
36	8 lines from bottom	$\dot{W}_{in} = (2 \text{ lb/min})(1 \text{ min}/60 \text{ s})[(119.20 - 107.471)] \text{ Btu/lb}$
36	7 lines from bottom	$= 0.391 \text{ Btu/s} = 1407 \text{ Btu/h}$

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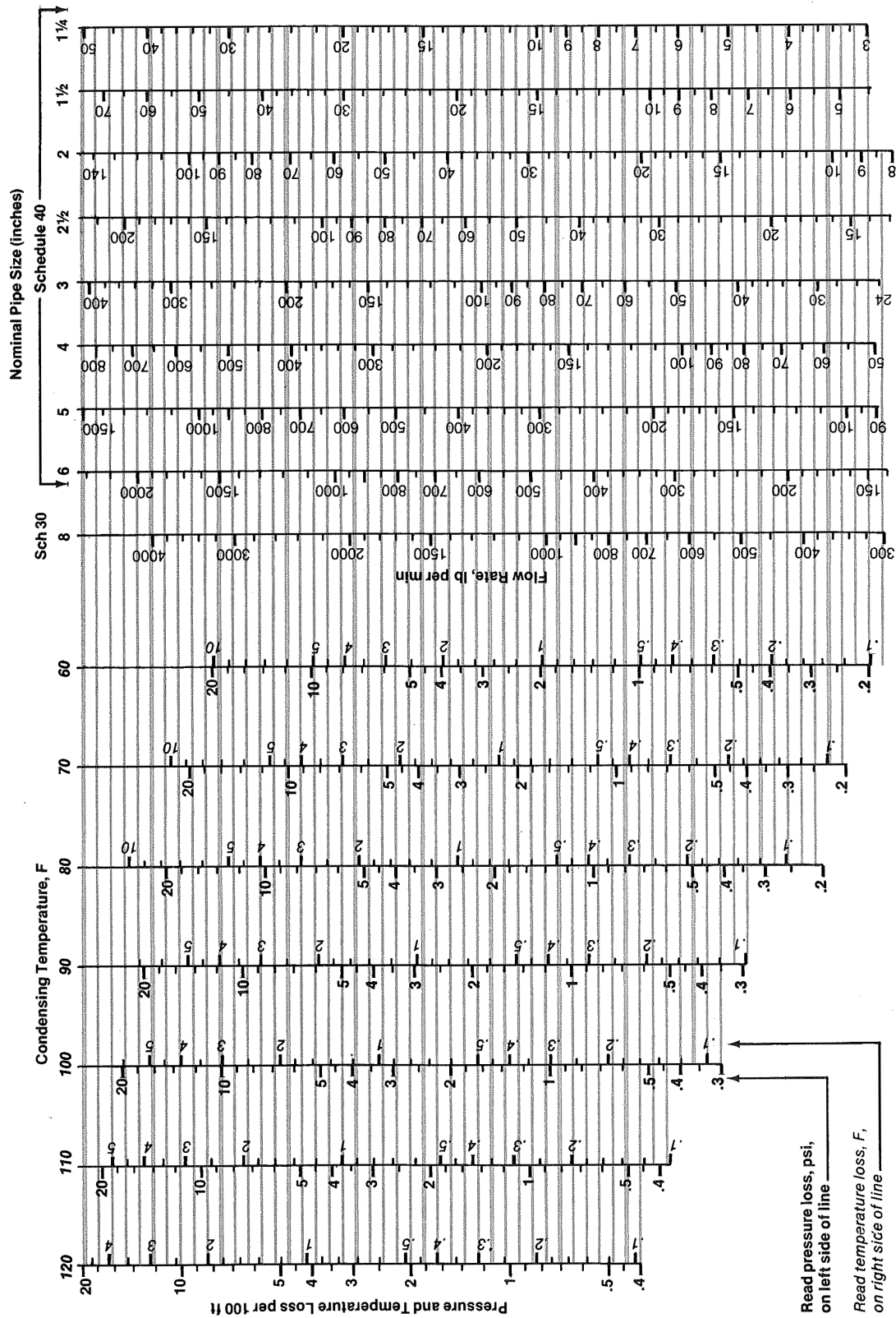
Page #	Location	
36	6 lines from bottom	$= (1407 \text{ Btu/h})\left(\frac{1}{2545 \text{ Btu/h}}\right) = 0.55 \text{ hp}$
37	Example 2-6	$h_2 = 24.72 \text{ Btu/lb}$
38	15 lines from top	$p_2(\text{sat.}) = 5.778 \text{ psia}$
38	18 lines from top	$h_1 = 30.671 \text{ Btu/lb} = h_2$
39	2 lines from top	$h_{f2} = 18.570 \text{ Btu/lb} \quad h_{g2} = 95.877 \text{ Btu/lb}$
39	4 lines from top	$= \frac{30.671 - 18.570}{95.877 - 18.570}$
39	5 lines from top	$= 0.157 \text{ or } 15.7\%$
40	2 lines from top	$h_1 = 30.671 \text{ Btu/lb} \quad h_2 = 95.877 \text{ Btu/lb}$
40	4 lines from top	$= (5 \text{ lb/min})(95.877 - 30.671) \text{ Btu/lb}$
48	8 lines from top	$\dot{W}_{out}$ should read $\dot{W}_c$
55	12 lines from top	After the first sentence insert: "Thus the results shown in Figure 3-9 include the removal of flash gas."
55	13 lines from top	"temperature is observed to be approximately"
55	13 lines from top	30°F should be 22°F.
55	14 lines from top	70 psia should be 60.1 psia.
55	15 lines from top	55 psia should be 70.0 psia, and 18°F should be 30°F.
55	17 lines from top	2% should be 4%
62	Example 3-3 solution	$h_1 = 617.590 \text{ Btu/lb}$ and $s_1 = 1.29629 \text{ Btu/lb}\cdot^\circ\text{R}$
82	15 and 16 lines from top	$\dot{Q} = \frac{kA}{x}(T_1 - T_2)$ where $\dot{Q}$ is the heat transfer rate... should read $Q = \frac{kA}{x}(T_1 - T_2)$ where $Q$ is the heat transfer rate...
89	First line	Change "13.8 ft <sup>3</sup> /lb dry air" to "13.8 ft <sup>3</sup> /lb dry air".
89	Example 4-2 solution	Change the last sentence of Example 4-2 solution to: "Because the can's surface temperature is less than the surrounding air's dew point temperature, moisture must condense on the can surface."
110	Skill Dev Exercise 4-3	Change "copper siheets" to "copper sheets".
110	Skill Dev Exercise 4-5	Change last sentence to read "Assume that the refrigerant enters the coil as a saturated liquid and leaves as a saturated vapor at 35°F with no pressure drop."
122	3 lines from top	$\Delta h_{actual} = \frac{(\text{hp})42.4(\text{Btu/min}\cdot\text{hp})}{m_{actual}} = \frac{(9)(42.4)}{47.78} = 7.99 \text{ Btu/lb}$
122	6 lines from top	Thus, $\eta_s = 6.69/7.99 = 0.84$ or $\eta_s = 84\%$ .
144–45	In text	All occurrences of "impellor" should be spelled "impeller."
171	Skill Dev Exercise 6-4	Change "ft <sup>3</sup> /lb" to "ft <sup>3</sup> /min" or "cfm"
176	Table 7-1	Row two, column two, the roughness factor should be 0.000005.
177	Example 7-1	Viscosity = $\mu = 0.0199 \text{ lb/ft}\cdot\text{h}$ (1 h/3600 s) = 0.00000553 = $5.53 \times 10^{-6} \text{ lb/ft}\cdot\text{s}$
178	Last line	$p_1 = 105 \text{ psig} + 14.7 \text{ psia} = 119.7 \text{ psia}$
179	4 lines from top	$= 119.7 - \left(76.58 \frac{\text{lb}}{\text{ft}^3}\right)(25 \text{ ft})\left(\frac{1 \text{ ft}^2}{144 \text{ in.}^2}\right)$
179	5 lines from top	$= 106.4 \text{ psia}$
181–82	Figures 7-3 and 7-4	Replace Figures 7-3 and 7-4 with more legible graphics as shown on the following pages.



Based on temperatures superheated above saturation as normally occurs in practice. See text for details.

Wall thicknesses used for this chart are not a design recommendation. Consult applicable codes and standards for safety limitations. See text for loss with other wall thicknesses.

**Figure 7-3 Pressure and temperature losses for ammonia in steel pipe suction lines.**



Based on temperatures superheated above saturation as normally occurs in practice. See text for details.

Wall thicknesses used for this chart are not a design recommendation. Consult applicable codes and standards for safety limitations. See text for loss with other wall thicknesses.

**Figure 7-4 Pressure and temperature losses for ammonia in steel pipe discharge lines.**

Page #	Location	
189	2 lines from top	Change “diagram given in Figure B-5” to “diagram given in Figure B-6”.
198	Skill Dev Exercise 7-1	Add the word “steel” in the first sentence as shown: “Calculate the pressure drop for a 100 ft length of a 6 in. steel Schedule 40 ammonia suction line.”
198	Skill Dev Exercise 7-3	Add the word “steel” in the first sentence as shown: “A steel piping layout for an ammonia liquid line is shown in the figure below....”
200	Skill Dev Exercise 7-6	Add the word “steel” in the first sentence as shown: “A recirculation system that uses ammonia as the refrigerant has an insulated steel line delivering liquid to a cluster of evaporators.”
231	Figure 9-1	Revise Figure 9-1 as shown on the following pages.
234	Equation 9-2	$V_f = A_f L \left[ \pi R^2 \left( \frac{\theta}{180^\circ} \right) - R(R - H_f) \sin \theta \right]$
248	Eight lines from bottom	Change $1.9 \times 1.9 = 3.61$ ft to $(2)(1.9$ ft) = 3.8 ft.
248	Seven lines from bottom	Change 3.6 ft 3.8 ft.
248	Three lines from bottom	Change 3.6 ft to 3.8 ft.
259	Figure 10-1	Revise Figure 10-1 as shown on the following pages.
265	Table 10-2	Seventh column, second row: 8.81 should be 10.36.
272	Last sentence	“The dominant code in the U.S. HVAC&R industry is ASHRAE Standard 15, which is continuously maintained by ASHRAE and consists of 13 sections and ten appendices.”
274	Example 10-1	$m = \frac{pV}{R_{R-404A} T}$ $= \frac{(14.7)(144)(69)}{(15.83)(70 + 460)}$ $= 17.4 \frac{\text{lb R-404A}}{1000 \text{ ft}^3}$
275	Third line from top	“See that the maximum allowed quantity of refrigerant R-404A, according to Table 10-1, is 2227 lb, which in this situation is far greater than the 45 lb charge.”
276	7 lines from top	44 should be 144
291–92	Solution	<p>Correct as follows:</p> <p>Furthermore, we can write</p> $\frac{M}{\Delta t} = \dot{m} \quad \text{and} \quad \frac{Q_{total}}{\Delta t} = \dot{Q}$ <p>where the dot above the quantity denotes a time rate of change or flow. Substituting <math>\dot{m}</math> and <math>\dot{Q}</math> into the above equation gives</p> $\dot{Q} = \dot{m} c_{p, unfrozen} (T_{initial} - T_{freeze}) + \dot{m} h_L + \dot{m} c_{p, frozen} (T_{freeze} - T_{final})$ <p>For this example, <math>\dot{m} = 200</math> lb/min, and from Appendix C, Table C-2, for blueberries, we have</p> $c_{p, unfrozen} = 0.91 \text{ Btu/lb}^\circ\text{F}$ $c_{p, frozen} = 0.49 \text{ Btu/lb}^\circ\text{F}$ $h_L = 122 \text{ Btu/lb}$ $T_{freeze} = 29.1^\circ\text{F}$ <p>So,</p> $\dot{Q} = (200)(0.91)(80 - 29.1) + (200)(122) + (200)(0.49)[29.1 - (-5)]$ $= 9264 + 24,400 + 3342$ $= 37,010 \text{ Btu/min}$ <p>or that</p> $\dot{Q} = \frac{37,010}{200} = 185 \text{ tons, refrigerating capacity}$

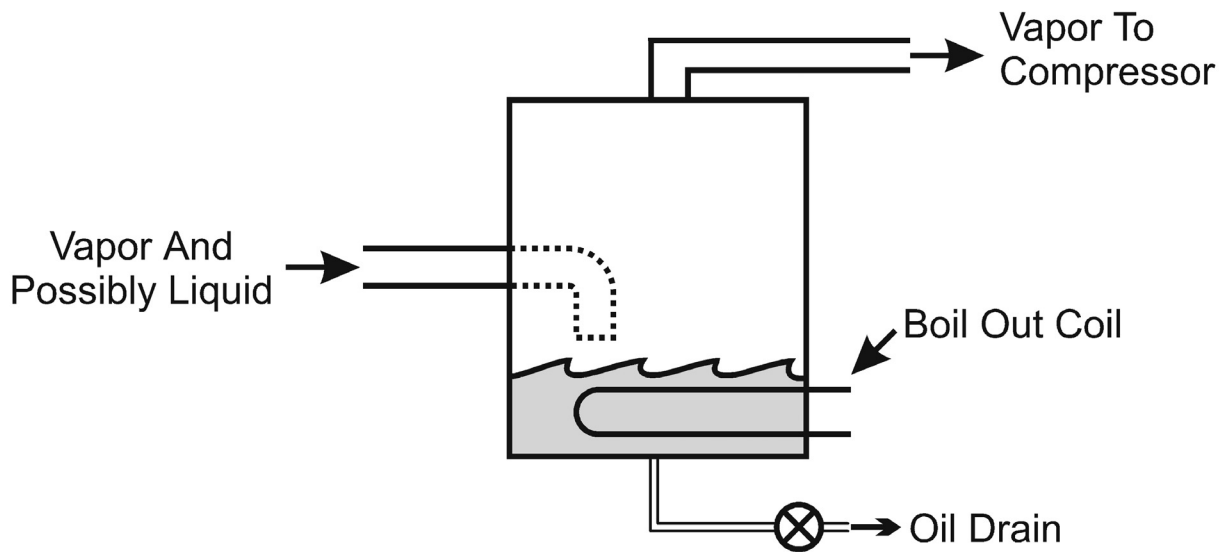
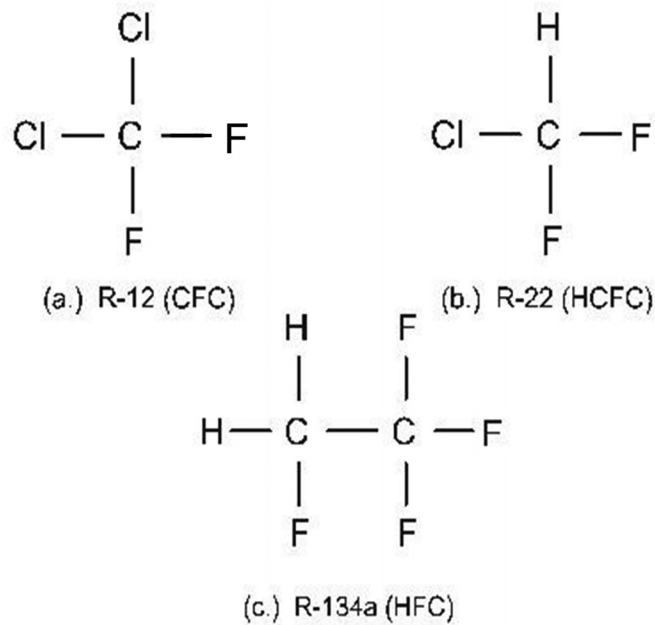


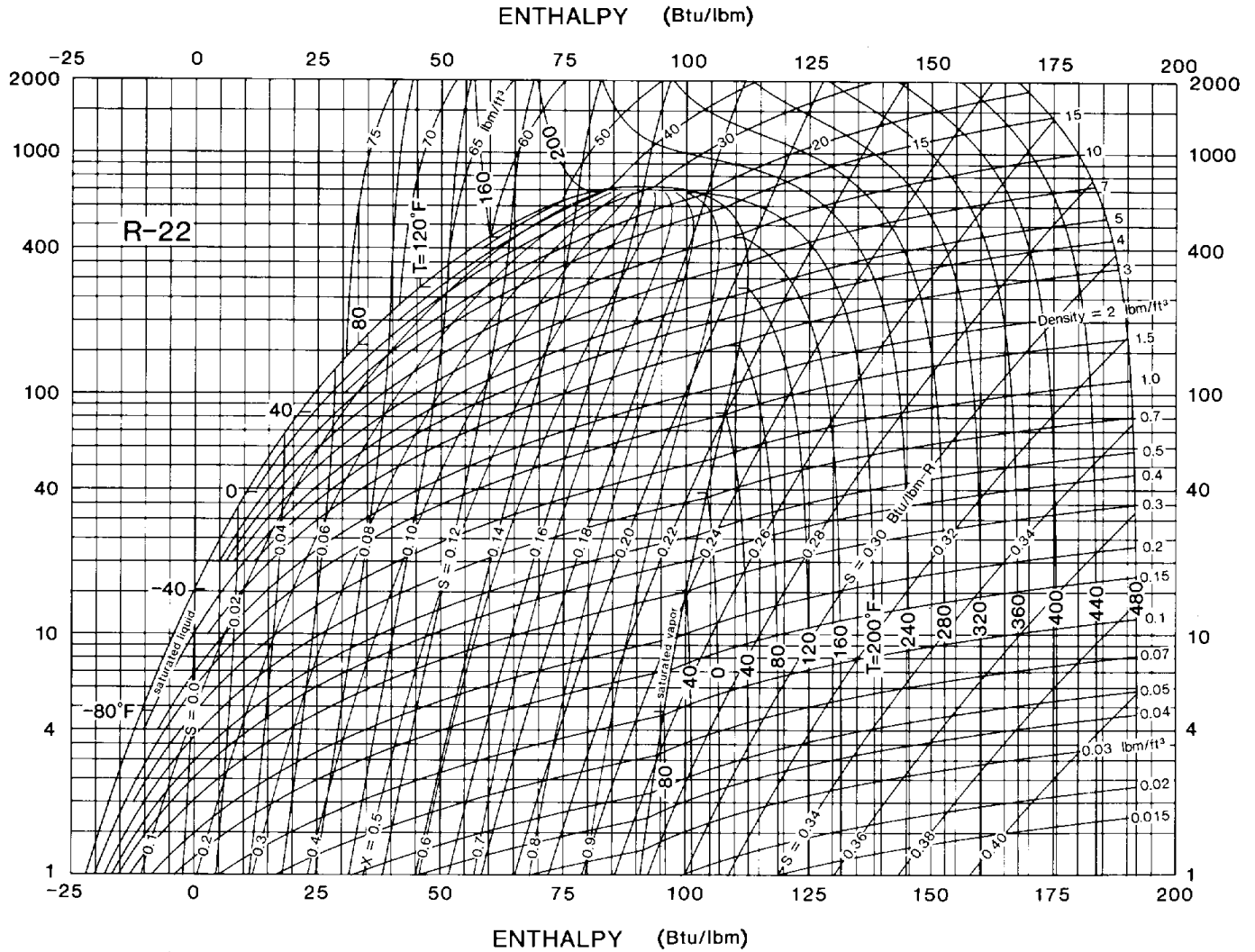
Figure 9-1 Suction line accumulator.



C (Carbon Atom), Cl (Chlorine Atom), F (Fluorine Atom)  
H (Hydrogen Atom), — (Chemical Bond)

Figure 10-1 Molecular structures of select halocarbon refrigerants.

Page #	Location	
293	2 lines from bottom	$h_c = 0.19V^{0.6}$ (Btu/h·ft <sup>2</sup> ·°F)
298	17 lines from bottom	Replace last part of paragraph with “Figure 11-7d shows the airflow pattern as horizontal with no baffling. Other spiral freezer designs use baffles to split and direct the airflow in a manner to decrease freezing times. Additionally, the airflow pattern may be arranged such that the coldest air first contacts the coldest product. This is generally referred to as a parallel arrangement.”
311	First three lines from top	$h_{am,in}(\text{sat. liq., } -20^\circ\text{F}) = 21.253 \text{ Btu/lb}$ $h_{am,out}(\text{sat. vap., } -20^\circ\text{F}) = 604.789 \text{ Btu/lb}$ $\dot{m}_{am} = \frac{(140 \text{ lb/min})(0.695 \text{ Btu/lb} \cdot ^\circ\text{F})[10^\circ\text{F} - (-5^\circ\text{F})]}{(604.789 - 21.253) \text{ Btu/lb}} = 2.50 \text{ lb/min}$
311	Last equation	Change the solution from “4050 Btu/lb·°F” to “4050 Btu/h·°F”.
313	References and Bibliography	Add the following as the first entry: ASHRAE. 1997. <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19. Atlanta: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc.
314	Skill Dev Exercise 11-5	Change 20,000 lb to 60,000 lb.
351	Skill Dev Exercise 12-5	Modify last paragraph to read: “Assuming that each month contains 30 days, what is the average daily leak rate of R-123 for each month? Is there reason for concern? Use the Internet to access the U.S. EPA regulations concerning refrigerant leak rates and determine if there is cause for concern. Is there another reason for concern?”
353	First line	Change 2009 to 1997.
354		Replace Table A-1 with the R-22 table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
355		Replace Table A-2 with the R-23 table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
356		Replace Table A-3 with the R-123 table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
357		Replace Table A-4 with the R-134a table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
358–59		Replace Table A-5 with the R-134a table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
360		Replace Table A-6 with the R-404A table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
361		Replace Table A-7 with the R-717 table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
362		Replace Table A-8 with the R-744 table from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
363	Second line	Change 2009 to 1997.
364		Replace Figure B-1 with the R-22 diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
365		Replace Figure B-2 with the R-23 diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
366		Replace Figure B-3 with the R-123 diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
367		Replace Figure B-4 with the R-134a diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
368		Replace Figure B-5 with the R-404A diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
369		Replace Figure B-6 with the R-717 diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.
370		Replace Figure B-7 with the R-744 diagram from 1997 <i>ASHRAE Handbook—Fundamentals</i> , Chapter 19, as shown on the following pages.



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Fig. 4 Pressure-Enthalpy Diagram for Refrigerant 22









Refrigerant 134a (1,1,1,2-Tetrafluoroethane) Properties of Saturated Liquid and Saturated Vapor

Table with columns for Temp, Pressure, Density, Volume, Enthalpy, Entropy, Specific Heat, Velocity of Sound, Viscosity, Thermal Cond, and Surface Tension. Rows list properties for temperatures from -153.94a to 213.85c.

\*temperatures are on the ITS-90 scale a = triple point b = normal boiling point c = critical point



Refrigerant 134a Properties of Superheated Vapor (Concluded)

Table with 15 columns: Pressure (psia), Saturation temperature (°F), Temp.\* (°F), Density (lb/ft³), Enthalpy (Btu/lb), Entropy (Btu/lb·°F), Vel. Sound (ft/s). The table is organized into 12 major sections for pressures: 225.00, 250.00, 275.00, 300.00, 325.00, 350.00, 375.00, 400.00, and 600.00 psia, with the last section for 600.00 psia labeled as supercritical.

\*temperatures are on the ITS-90 scale

Refrigerant 404A [R-125/143a/134a (44/52/4)] Properties of Liquid on the Bubble Line and Vapor on the Dew Line

Pressure, psia	Temperature*, °F		Density, lb/ft <sup>3</sup> Liquid	Volume, ft <sup>3</sup> /lb Vapor	Enthalpy, Btu/lb		Entropy, Btu/lb·°F		Specific Heat $c_p$ , Btu/lb·°F		$c_p/c_v$	Velocity of Sound, ft/s		Pressure, psia
	Bubble	Dew			Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		Liquid	Vapor	
1.00	-130.49	-128.46	89.51	36.17	-25.81	71.15	-0.06905	0.22497	0.2733	0.1535	1.160	3217.	439.5	1.00
1.50	-120.93	-119.01	88.60	24.74	-23.19	72.53	-0.06119	0.22089	0.2756	0.1568	1.159	3113.	444.4	1.50
2.00	-113.74	-111.89	87.91	18.90	-21.20	73.57	-0.05539	0.21811	0.2774	0.1593	1.158	3037.	447.9	2.00
2.50	-107.91	-106.11	87.35	15.34	-19.58	74.42	-0.05074	0.21604	0.2788	0.1614	1.158	2978.	450.6	2.50
3.00	-102.97	-101.22	86.86	12.94	-18.20	75.14	-0.04685	0.21440	0.2801	0.1633	1.158	2928.	452.8	3.00
4.00	-94.84	-93.16	86.06	9.888	-15.91	76.32	-0.04051	0.21192	0.2821	0.1664	1.158	2848.	456.3	4.00
5.00	-88.22	-86.59	85.41	8.027	-14.04	77.29	-0.03543	0.21008	0.2838	0.1690	1.158	2785.	458.9	5.00
6.00	-82.60	-81.02	84.84	6.768	-12.44	78.11	-0.03116	0.20863	0.2853	0.1712	1.159	2731.	461.0	6.00
7.00	-77.69	-76.15	84.35	5.859	-11.03	78.83	-0.02746	0.20746	0.2867	0.1733	1.159	2685.	462.7	7.00
8.00	-73.32	-71.80	83.90	5.171	-9.77	79.46	-0.02419	0.20647	0.2879	0.1751	1.160	2643.	464.1	8.00
10.00	-65.74	-64.28	83.12	4.195	-7.58	80.56	-0.01858	0.20488	0.2901	0.1784	1.161	2573.	466.4	10.00
12.00	-59.29	-57.86	82.45	3.535	-5.70	81.50	-0.01386	0.20365	0.2921	0.1813	1.163	2513.	468.1	12.00
14.00	-53.64	-52.25	81.86	3.059	-4.04	82.31	-0.00976	0.20266	0.2938	0.1839	1.165	2461.	469.5	14.00
14.696b	-51.82	-50.44	81.67	2.922	-3.51	82.57	-0.00845	0.20235	0.2944	0.1848	1.165	2445.	469.9	14.70
16.00	-48.59	-47.23	81.32	2.697	-2.55	83.03	-0.00613	0.20183	0.2954	0.1864	1.166	2415.	470.5	16.00
18.00	-44.02	-42.69	80.84	2.414	-1.20	83.69	-0.00286	0.20113	0.2969	0.1886	1.168	2373.	471.4	18.00
20.00	-39.83	-38.52	80.38	2.185	0.05	84.28	0.00012	0.20052	0.2983	0.1907	1.170	2335.	472.0	20.00
22.00	-35.95	-34.66	79.96	1.997	1.21	84.83	0.00286	0.19999	0.2997	0.1927	1.172	2300.	472.6	22.00
24.00	-32.34	-31.07	79.57	1.839	2.30	85.34	0.00541	0.19951	0.3009	0.1945	1.174	2267.	473.0	24.00
26.00	-28.95	-27.71	79.19	1.704	3.32	85.81	0.00778	0.19909	0.3022	0.1963	1.175	2237.	473.3	26.00
28.00	-25.77	-24.54	78.84	1.588	4.29	86.26	0.01001	0.19871	0.3033	0.1981	1.177	2208.	473.5	28.00
30.00	-22.75	-21.54	78.50	1.487	5.21	86.68	0.01210	0.19837	0.3045	0.1997	1.179	2181.	473.7	30.00
32.00	-19.88	-18.68	78.18	1.398	6.08	87.07	0.01409	0.19805	0.3056	0.2013	1.181	2155.	473.8	32.00
34.00	-17.15	-15.97	77.87	1.319	6.92	87.45	0.01598	0.19776	0.3066	0.2029	1.183	2130.	473.8	34.00
36.00	-14.54	-13.37	77.57	1.249	7.72	87.80	0.01778	0.19750	0.3077	0.2044	1.185	2106.	473.8	36.00
38.00	-12.04	-10.88	77.28	1.186	8.50	88.14	0.01950	0.19725	0.3087	0.2059	1.187	2084.	473.8	38.00
40.00	-9.64	-8.49	77.00	1.129	9.24	88.47	0.02115	0.19702	0.3097	0.2073	1.188	2062.	473.7	40.00
42.00	-7.33	-6.19	76.73	1.077	9.96	88.78	0.02273	0.19681	0.3106	0.2087	1.190	2041.	473.5	42.00
44.00	-5.10	-3.97	76.47	1.030	10.65	89.08	0.02425	0.19661	0.3116	0.2101	1.192	2021.	473.4	44.00
46.00	-2.94	-1.83	76.22	0.9864	11.33	89.37	0.02572	0.19642	0.3125	0.2115	1.194	2002.	473.2	46.00
48.00	-0.86	0.24	75.97	0.9465	11.98	89.64	0.02713	0.19624	0.3134	0.2128	1.196	1983.	473.0	48.00
50.00	1.16	2.25	75.73	0.9098	12.62	89.91	0.02850	0.19607	0.3143	0.2141	1.198	1965.	472.8	50.00
55.00	5.94	7.01	75.16	0.8292	14.13	90.53	0.03174	0.19569	0.3166	0.2172	1.203	1921.	472.1	55.00
60.00	10.41	11.46	74.61	0.7616	15.55	91.11	0.03476	0.19535	0.3187	0.2203	1.208	1881.	471.3	60.00
65.00	14.61	15.64	74.09	0.7040	16.89	91.65	0.03758	0.19505	0.3208	0.2233	1.213	1843.	470.5	65.00
70.00	18.57	19.58	73.60	0.6543	18.17	92.14	0.04023	0.19478	0.3229	0.2262	1.218	1807.	469.5	70.00
75.00	22.32	23.31	73.12	0.6111	19.39	92.61	0.04274	0.19453	0.3249	0.2290	1.223	1773.	468.5	75.00
80.00	25.88	26.86	72.66	0.5731	20.55	93.05	0.04511	0.19430	0.3269	0.2318	1.228	1740.	467.4	80.00
85.00	29.28	30.25	72.22	0.5393	21.67	93.46	0.04738	0.19409	0.3288	0.2345	1.233	1709.	466.3	85.00
90.00	32.54	33.49	71.79	0.5092	22.74	93.85	0.04954	0.19389	0.3308	0.2372	1.239	1679.	465.1	90.00
95.00	35.66	36.59	71.37	0.4822	23.78	94.21	0.05162	0.19370	0.3327	0.2399	1.244	1651.	463.9	95.00
100.00	38.66	39.58	70.97	0.4577	24.78	94.56	0.05361	0.19353	0.3347	0.2426	1.250	1623.	462.7	100.00
110.00	44.34	45.24	70.19	0.4152	26.69	95.20	0.05737	0.19320	0.3385	0.2479	1.261	1571.	460.1	110.00
120.00	49.65	50.52	69.44	0.3796	28.50	95.79	0.06088	0.19290	0.3424	0.2531	1.273	1521.	457.4	120.00
130.00	54.63	55.48	68.72	0.3492	30.21	96.31	0.06417	0.19262	0.3463	0.2584	1.285	1475.	454.6	130.00
140.00	59.34	60.17	68.02	0.3230	31.84	96.80	0.06728	0.19235	0.3502	0.2638	1.298	1431.	451.7	140.00
150.00	63.80	64.61	67.35	0.3001	33.41	97.24	0.07023	0.19209	0.3542	0.2692	1.312	1389.	448.8	150.00
160.00	68.05	68.83	66.69	0.2800	34.91	97.64	0.07304	0.19184	0.3583	0.2747	1.326	1349.	445.7	160.00
170.00	72.10	72.87	66.05	0.2622	36.36	98.01	0.07573	0.19159	0.3624	0.2803	1.341	1311.	442.7	170.00
180.00	75.97	76.73	65.41	0.2462	37.76	98.35	0.07830	0.19134	0.3667	0.2861	1.357	1274.	439.6	180.00
190.00	79.69	80.43	64.79	0.2319	39.12	98.66	0.08077	0.19109	0.3711	0.2921	1.374	1238.	436.4	190.00
200.00	83.27	83.99	64.18	0.2189	40.44	98.94	0.08316	0.19084	0.3757	0.2982	1.391	1203.	433.2	200.00
220.00	90.04	90.72	62.99	0.1963	42.98	99.42	0.08769	0.19032	0.3853	0.3113	1.430	1138.	426.7	220.00
240.00	96.36	97.01	61.81	0.1772	45.39	99.82	0.09196	0.18978	0.3957	0.3256	1.474	1076.	420.1	240.00
260.00	102.29	102.92	60.64	0.1610	47.71	100.12	0.09600	0.18921	0.4072	0.3414	1.524	1016.	413.3	260.00
280.00	107.90	108.49	59.48	0.1468	49.95	100.35	0.09985	0.18860	0.4200	0.3592	1.582	960.	406.4	280.00
300.00	113.20	113.77	58.32	0.1344	52.12	100.49	0.10355	0.18794	0.4345	0.3796	1.650	906.	399.4	300.00
320.00	118.24	118.78	57.15	0.1234	54.24	100.55	0.10712	0.18722	0.4511	0.4032	1.730	853.	392.2	320.00
340.00	123.04	123.56	55.96	0.1136	56.31	100.53	0.11058	0.18643	0.4705	0.4310	1.827	803.	385.0	340.00
360.00	127.63	128.12	54.75	0.1047	58.35	100.43	0.11395	0.18557	0.4937	0.4646	1.945	753.	377.7	360.00
380.00	132.02	132.49	53.49	0.0965	60.37	100.23	0.11726	0.18461	0.5220	0.5061	2.092	705.	370.2	380.00
400.00	136.24	136.67	52.19	0.0890	62.38	99.94	0.12053	0.18353	0.5579	0.5588	2.282	657.	362.6	400.00
450.00	146.06	146.42	48.56	0.0722	67.49	98.62	0.12873	0.18011	0.7133	0.7888	3.120	541.	343.1	450.00
500.00	154.99	155.25	43.76	0.0565	73.20	95.88	0.13774	0.17463	1.2479	1.5641	5.974	422.	322.1	500.00
548.18c	162.50	162.50	35.84	0.0279	80.83	80.83	0.14972	0.14972	∞	∞	∞	0.	0.0	548.18

\*temperatures are on the ITS-90 scale

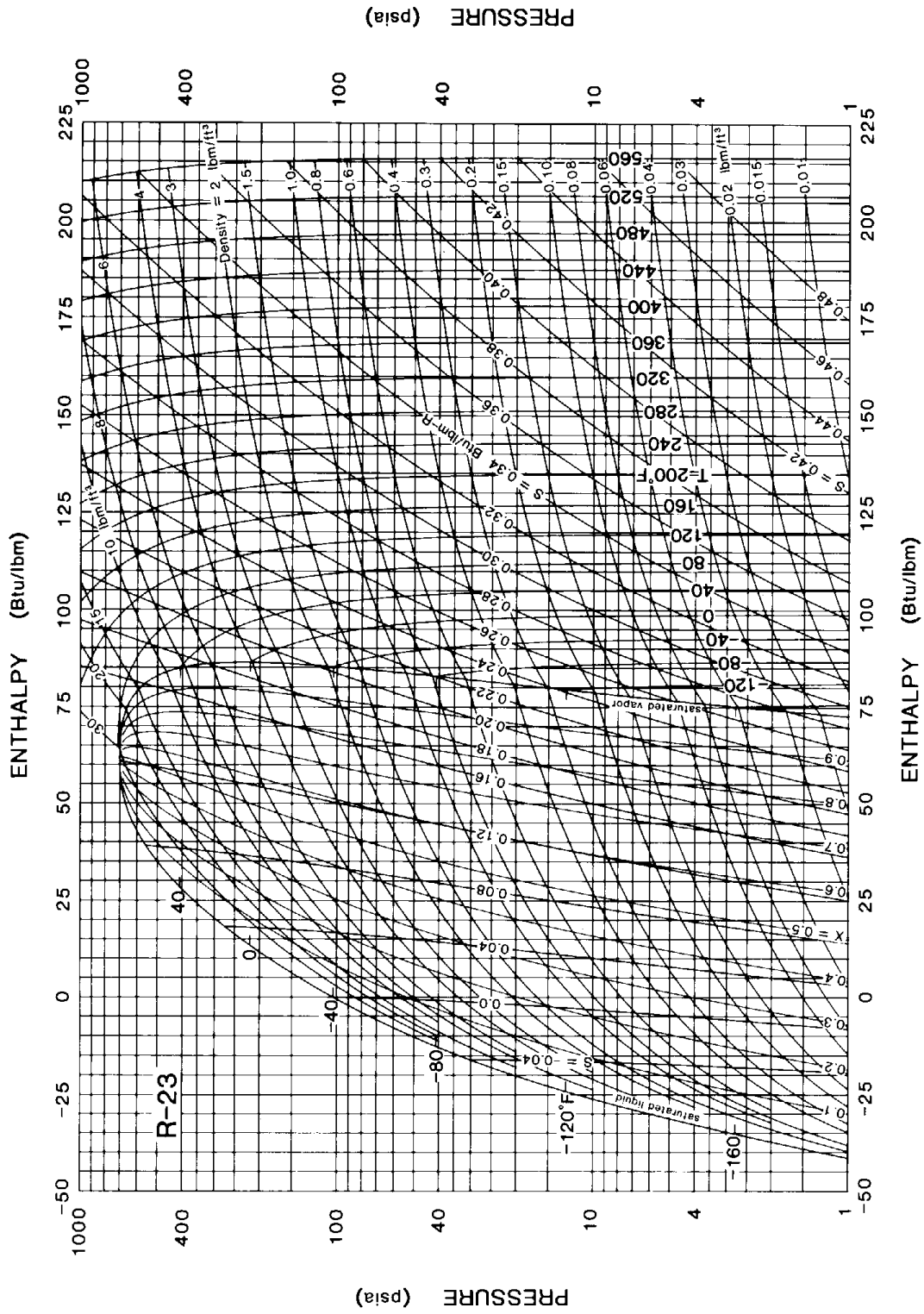
b = one standard atmosphere

c = critical point



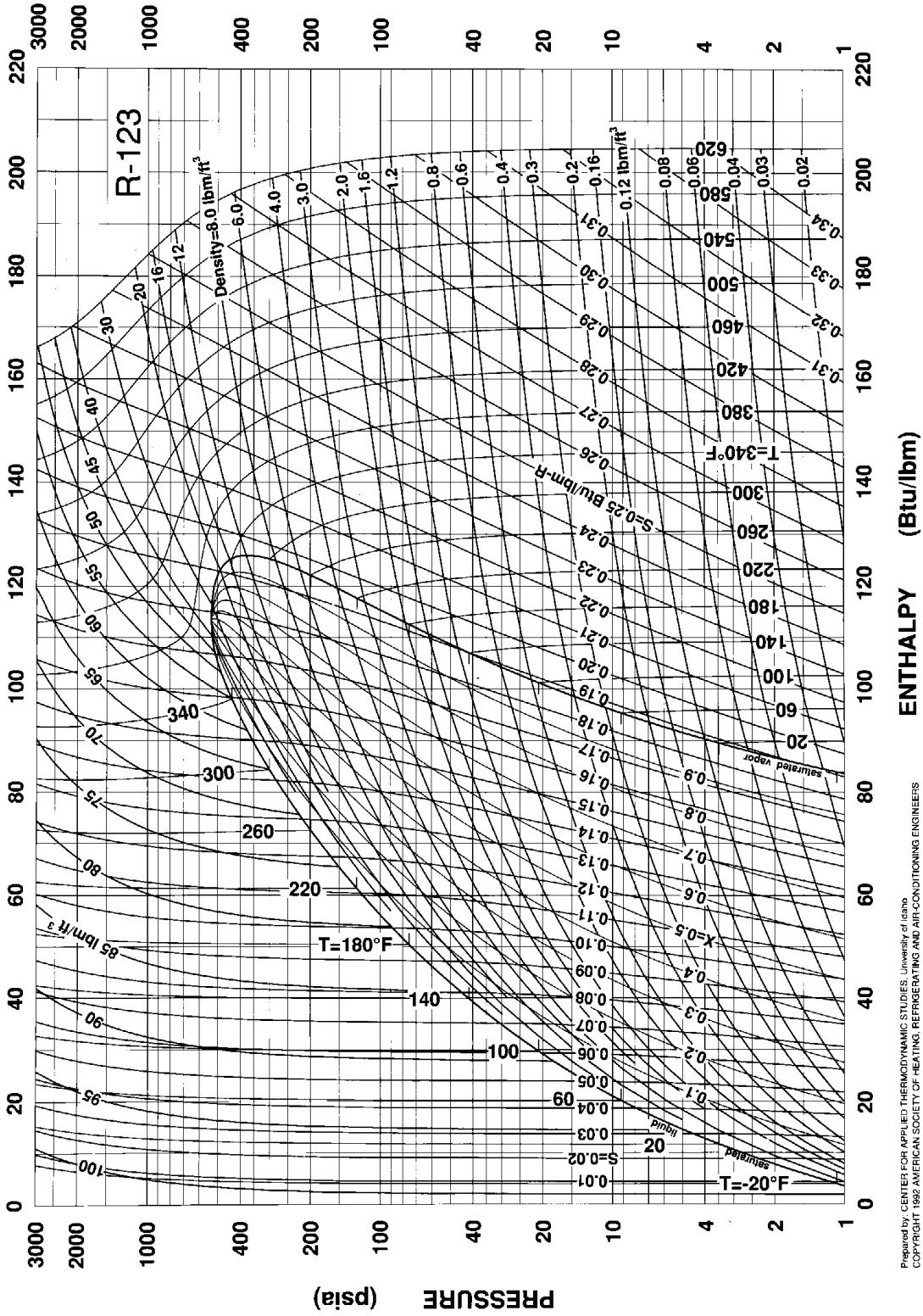






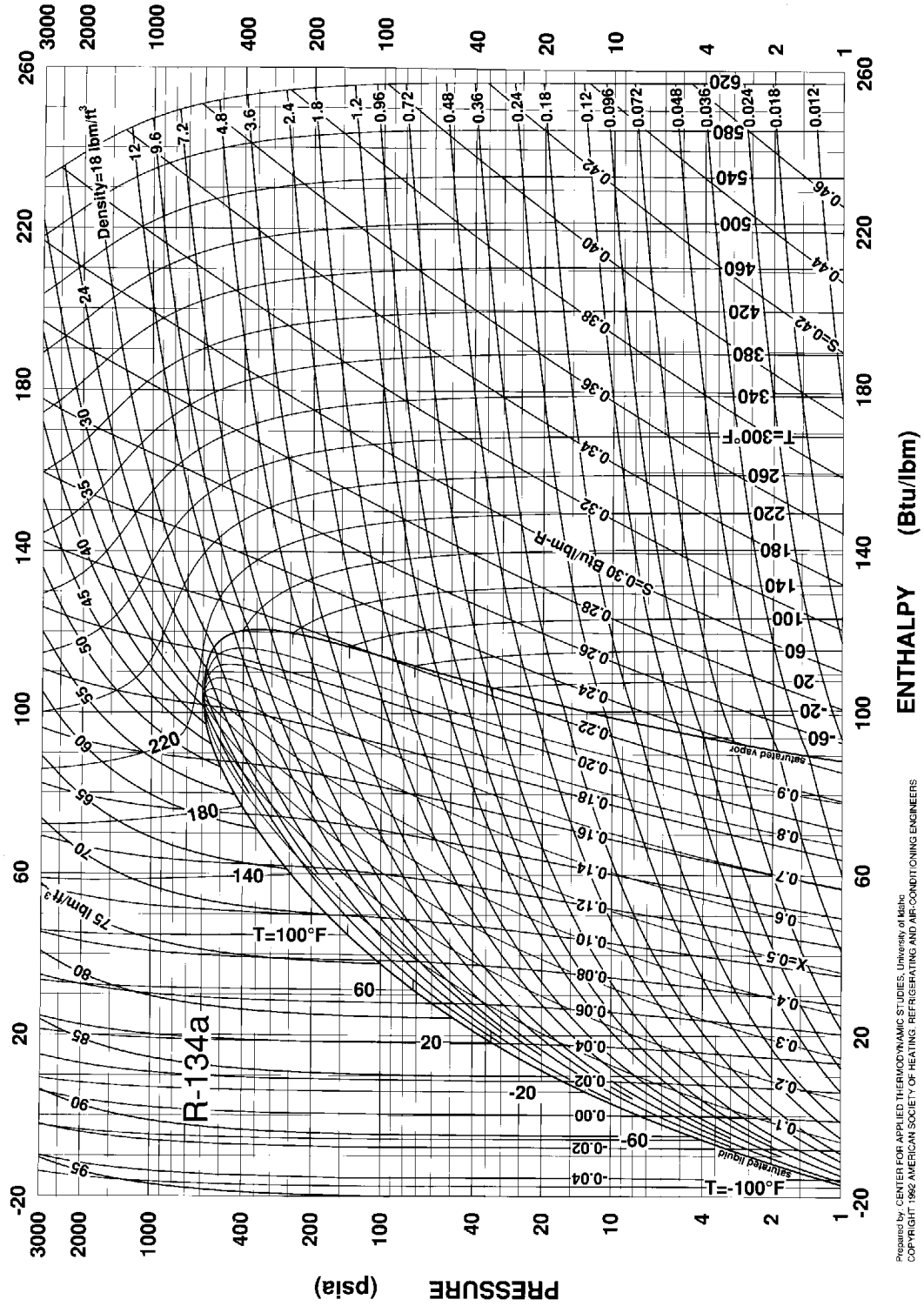
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Fig. 5 Pressure-Enthalpy Diagram for Refrigerant 23



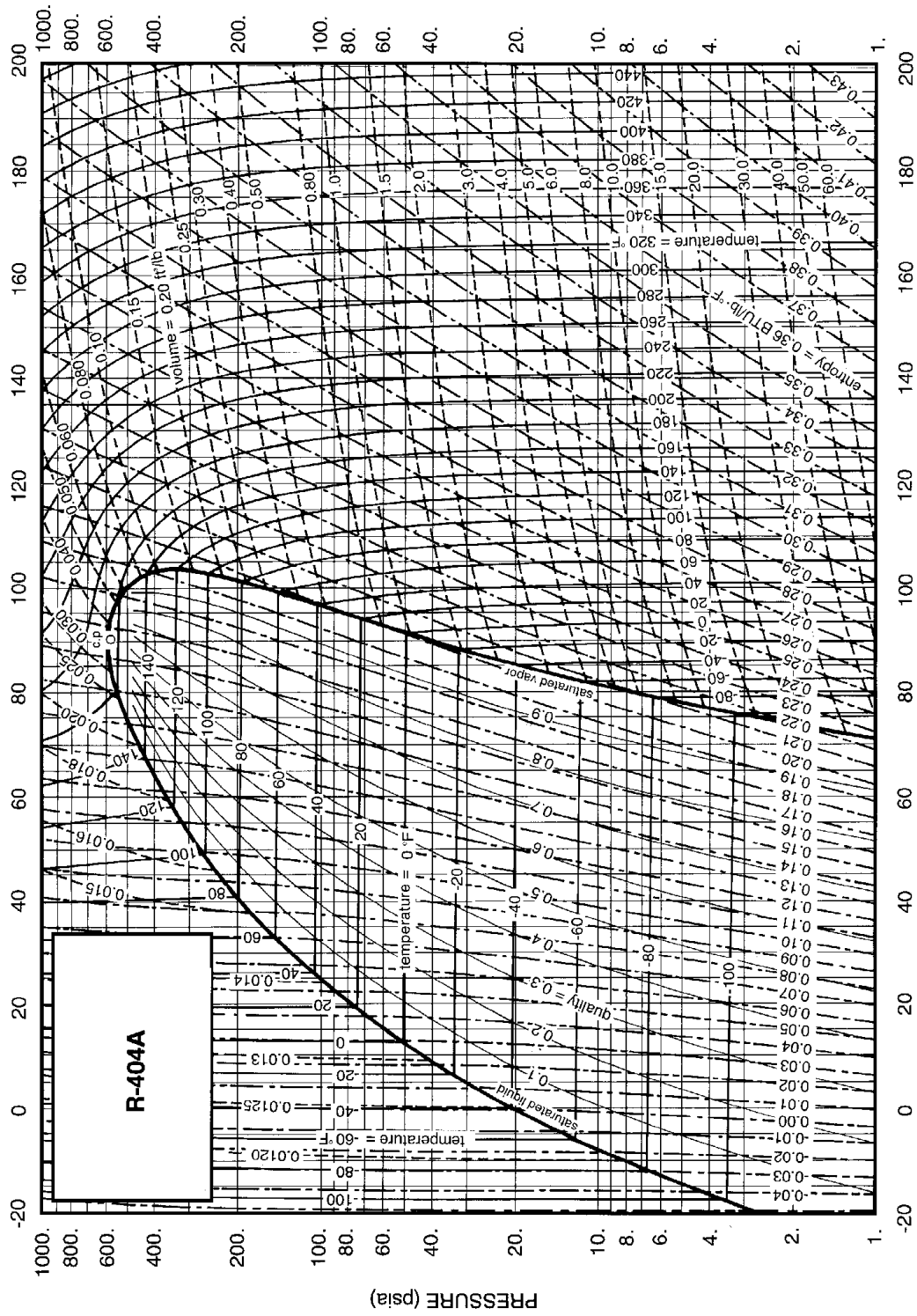
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Fig. 9 Pressure-Enthalpy Diagram for Refrigerant 123

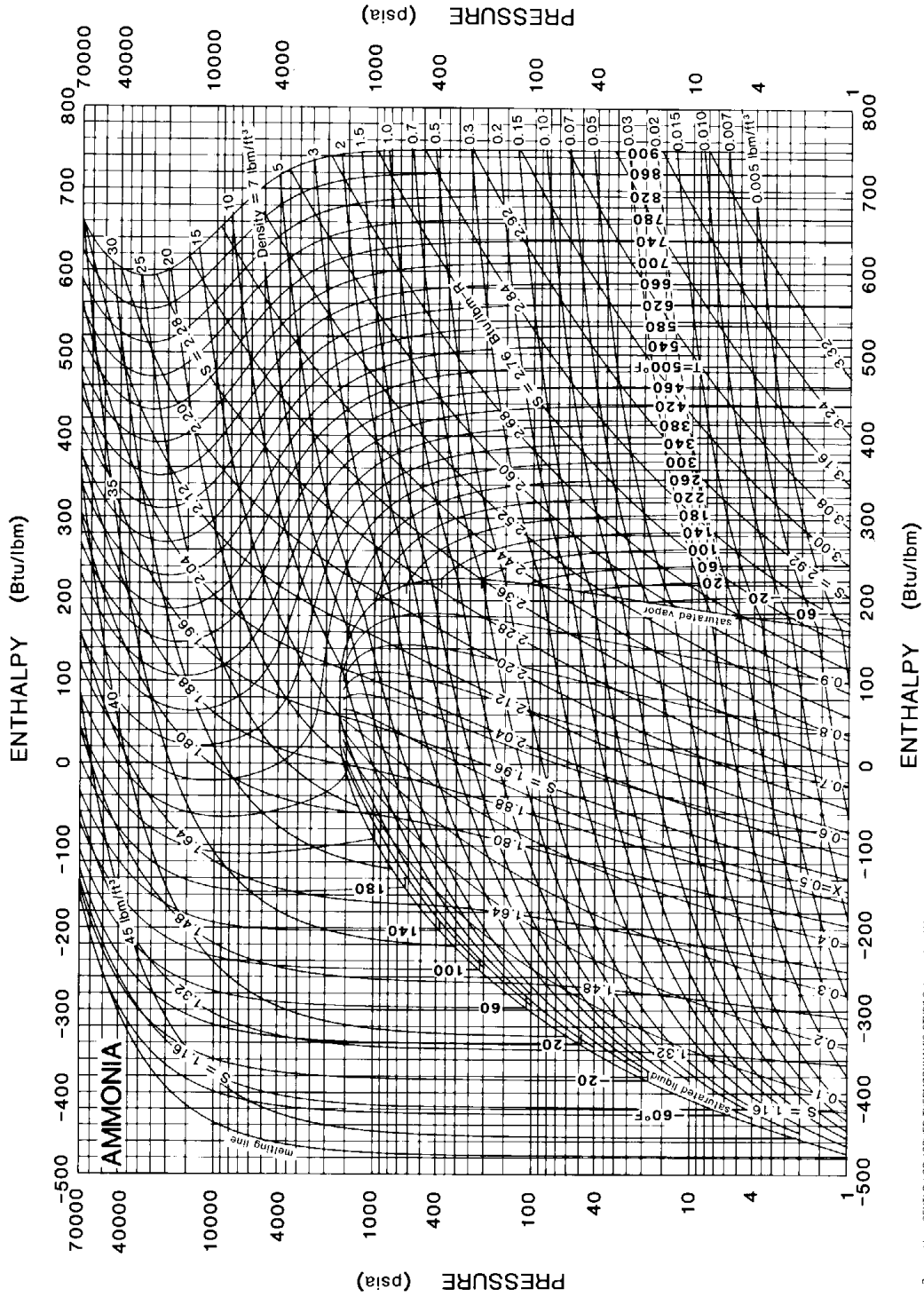


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Fig. 12 Pressure-Enthalpy Diagram for Refrigerant 134a

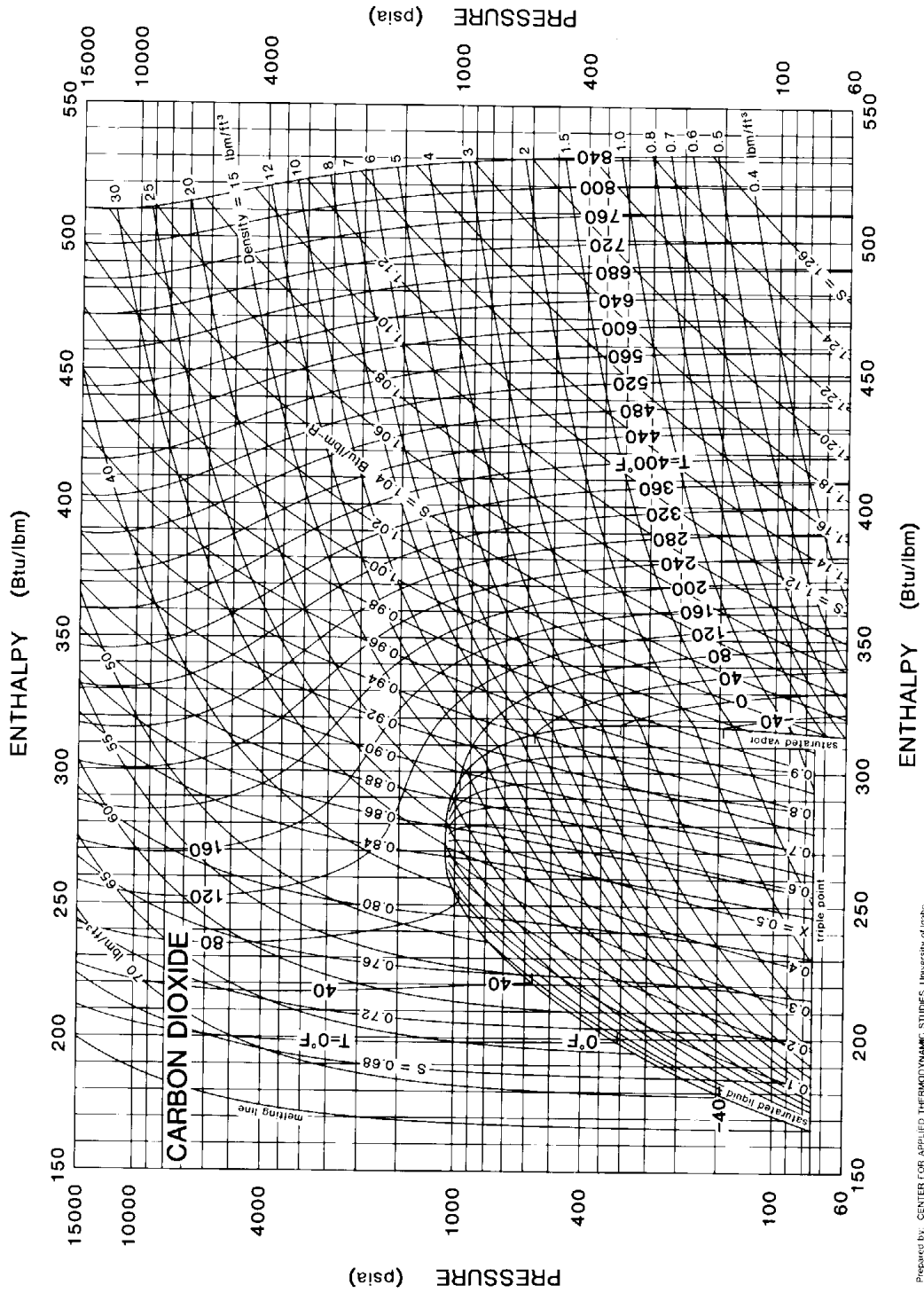


**ENTHALPY (Btu/lbm)**  
**Fig. 16 Pressure-Enthalpy Diagram for Refrigerant 404A**  
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**Fig. 21 Pressure-Enthalpy Diagram for Refrigerant 717 (Ammonia)**  
 Note: The reference states for enthalpy and entropy differ from those in the table.

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**Fig. 23 Pressure-Enthalpy Diagram for Refrigerant 744 (Carbon Dioxide)**  
 Note: The reference states for enthalpy and entropy differ from those in the table.